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# Numerical study of the physical and chemical effects of hydrogen addition on laminar premixed combustion characteristics of methane and ethane

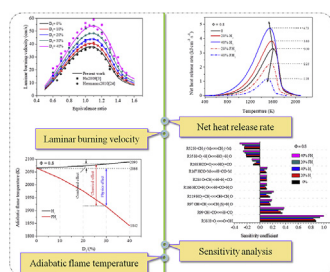
Longkai Xiang<sup>a</sup>, Hantao Jiang<sup>a</sup>, Fei Ren<sup>a,b</sup>, Huaqiang Chu<sup>a,\*</sup>,  
Pan Wang<sup>c,\*\*</sup>

<sup>a</sup> School of Energy and Environment, Anhui University of Technology, Ma'anshan, 243002, China

<sup>b</sup> Key Lab. for Power Machinery and Engineering of M. O. E., Shanghai Jiao Tong University, Shanghai, 200240, China

<sup>c</sup> School of Automotive and Traffic Engineering, Jiangsu University, Zhenjiang, 212013, China

## GRAPHICAL ABSTRACT



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## ABSTRACT

Methane and ethane are taken as the research objects. Using H<sub>2</sub> as diluent, based on Chemkin II/Premix Code and modified detailed chemical reaction mechanism: GRI 3.0\*-Mech (introducing three hypothetical substances of FH<sub>2</sub>, FO<sub>2</sub> and FN<sub>2</sub>), the physical and chemical effects of hydrogen on laminar burning velocities (LBVs), adiabatic flame temperatures (AFTs), net heat release rates (NHRRs) and elementary reactions responsible for temperature changes of two alkanes under different equivalence ratios were analyzed and determined. Results showed that the chemical effect of H<sub>2</sub> promotes the LBVs and AFTs of methane and ethane, while the physical effect decreases the two parameters. In addition, the physical effects of H<sub>2</sub> inhibit the chemical reactions of methane and ethane, resulting in the decrease of NHRRs. The chemical effect of H<sub>2</sub> accelerates the process of chemical reaction and obviously increases the NHRRs. The two most vital elementary reactions that promote the temperature rise of methane and ethane are  $\text{H} + \text{O}_2 \rightleftharpoons \text{OH} + \text{O}$  and  $\text{CO} + \text{OH}$ .

\* Corresponding author. School of Energy and Environment, Anhui University of Technology, Ma'anshan, 243002, China.

\*\* Corresponding author. School of Automotive and Traffic Engineering, Jiangsu University, Zhenjiang, 212013, China.

E-mail addresses: [hqchust@163.com](mailto:hqchust@163.com) (H. Chu), [wangpan@ujs.edu.cn](mailto:wangpan@ujs.edu.cn) (P. Wang).

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$\rightleftharpoons \text{H} + \text{CO}_2$ . The important reactions responsible for inhibiting the temperature rise are  $\text{H} + \text{CH}_3(+\text{M}) \rightleftharpoons \text{CH}_4(+\text{M})$  and  $\text{H} + \text{O}_2 + \text{H}_2\text{O} \rightleftharpoons \text{HO}_2 + \text{H}_2\text{O}$ .

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## Introduction

Fuel combustion is the main way of energy acquisition. Policy and social pressures have led to a shift in energy structure towards cleaner and lower carbon. However, the main energy sources for decades to come still have to rely on biomass energy and traditional fossil energy, which mainly composed of hydrocarbon fuels. At present, natural gas (NG) is seen as the most potential clean alternative energy source among conventional energy sources and renewable energy such as coal, oil, natural gas and ethanol [1–5]. Main component of natural gas is methane ( $\text{CH}_4$ ) and ethane ( $\text{C}_2\text{H}_6$ ), and because natural gas is produced in different places, natural gas varies in composition ratio [6–8], for example, the proportion of methane in natural gas produced in Liaohe, China is 97.05%, while the natural gas in Abu Dhabi is mainly composed of 82% methane and nearly 16% ethane, and natural gas produced in the USA consists mainly of 85% methane and 14% ethane. In fact, the combustion of natural gas in air still produces atmospheric pollutants, such as soot and  $\text{NO}_x$  [9,10]. Hydrogen Enriched Compressed Natural Gas (HCNG), also known as Hythane, is a feasible way to transfer to hydrogen energy. The mixture of natural gas and hydrogen can complement each other as engine fuel. Hydrogen addition improves the combustion performance of natural gas, reduces carbon emissions and broadens its ignition limit. The existence of natural gas makes up for the problems of fast combustion rate of hydrogen, low ignition energy and prone to premature ignition, deflagration and tempering.

Laminar combustion theory is the basis of studying turbulent combustion, and the combustion characteristics of laminar premixed combustion can directly reflect the essential characteristics of target fuel. For example, Laminar burning velocity (LBV) is the inherent characteristic of hydrocarbon fuel and an important parameter for laminar flame propagation and stability. Some researches [6,10] show that ethane blending into methane fuel can effectively enhance its laminar premixed combustion characteristics, such as laminar combustion speed, which may be one of the main reasons why laminar combustion speed of natural gas is faster than methane. There are two major reasons account for adding ethane can enhance LBV of methane. The first factor that the LBV of ethane is faster than LBV of methane [11,12]. With the increase of ethane doping ratio, the main fuel is changed from methane to ethane. Therefore, the laminar burning speed of the mixed fuel is increased. The other mainly point is that ethane will be cleaved into two methyl groups [13], which will greatly increase the concentration of important intermediate radicals and increase the reaction rate of  $\text{HO}_2 + \text{CH}_3 \rightleftharpoons \text{OH} + \text{CH}_3\text{O}$  and  $\text{OH} + \text{CH}_3 \rightleftharpoons \text{CH}_2(\text{S}) + \text{H}_2\text{O}$ . These two reactions can promote the oxidation of methane,

thereby improving the laminar burning velocity of methane. In recent years, many scholars have researched on the laminar combustion characteristics of methane and ethane.

Drrenberger et al. [6] utilized heat flux method (HFM) to measure the adiabatic LBVs of natural gas and  $\text{C}_1$ – $\text{C}_4$  alkanes flat flames under hydrogen doping ratio (0–40%), and summarized the correlations applied to LBV predictions of methane/ethane, methane-ethane mixtures and natural gas surrogate mixtures.

By HFM, Nilsson et al. [14] studied the LBVs of  $\text{CH}_4$  mixed with  $\text{C}_2\text{H}_6$ ,  $\text{C}_3\text{H}_8$  respectively, and the LBVs of their binary/ternary mixtures mixed with hydrogen were also measured. It was found that the LBVs of  $\text{CH}_4$  mixed with  $\text{C}_2\text{H}_6/\text{C}_3\text{H}_8$  and their binary and ternary mixtures is higher than that of pure  $\text{CH}_4$ . Konnov's research group measured the non-stretching adiabatic LBVs of  $\text{CH}_4/\text{N}_2/\text{O}_2$  [15],  $\text{CH}_4/\text{O}_2/\text{CO}_2$  [16],  $\text{C}_2\text{H}_6/\text{N}_2/\text{O}_2$  and  $\text{C}_2\text{H}_6/\text{Ar}/\text{O}_2$  [17] in laminar premixed flames at different oxygen concentrations by HFM. The LBVs of stable flat flame of  $\text{CH}_4/\text{O}_2/\text{CO}_2$  [18],  $\text{C}_2\text{H}_6/\text{CO}_2/\text{O}_2$  [19] and  $\text{CH}_4$  ( $\text{C}_2\text{H}_6/\text{C}_3\text{H}_8$ )/ $\text{CO}_2/\text{O}_2$  [20] at a given oxygen concentration ranges (31.55–35%). Coppens et al. [21] experimentally and numerically analyzed the LBV and NO formation of methane doped with hydrogen in laminar premixed flame. In addition, Konnov et al. measured the adiabatic LBV of  $(\text{CH}_4 + \text{H}_2)/\text{N}_2/\text{O}_2$  at low pressure [22], and summarized and analyzed the influence of initial temperature on the LBVs of  $\text{CH}_4/\text{N}_2/\text{O}_2$  and  $\text{H}_2/\text{N}_2/\text{O}_2$  [23]. Hermanns et al. [24] and Coppens et al. [25] experimentally studied the effects of temperature and mixture composition on LBV and NO formation of  $(\text{CH}_4 + \text{H}_2)/\text{N}_2/\text{O}_2$ . Goswami et al. also measured the LBVs of  $\text{CH}_4$  at different pressures (1–5 atm) [26]. Then the LBVs of  $\text{C}_2\text{H}_6$  and  $\text{C}_3\text{H}_8$  at 1–4 bar were measured and compared [27]. Based on the accurate experimental results, the correlations between LBV and pressure were deduced. Hu et al. [3,28,29] and Wang et al. [4,30], based on spherical propagation flame (SPF), a systematical and numerical study had carried out the laminar premixed flame combustion characteristics of  $\text{CH}_4$  under the condition of hydrogen addition. It was indicated that with the hydrogen doping ratios increasing, the non-stretching LBV and flame temperature increased, and the equivalence ratio of the maximum LBV also increased with the increasing of hydrogen content. The relationships between critical equivalence ratio for peak pressure rise rate and the ratio of  $\text{H}_2$  in syngas ( $\text{CO} + \text{H}_2$ ) and explosion characteristics of  $\text{H}_2$  ratio in  $\text{CH}_4/\text{H}_2/\text{Air}$  has been experimentally studied by Sun [31,32]. Ren et al. [33–35] conducted numerical analysis on the effects of different hydrogen doping ratios on the laminar premixed combustion characteristics of natural gas and the effects of  $\text{CO}_2$  and  $\text{H}_2\text{O}$  on the formation of intermediate  $\text{H}_2$  in methane/air flame and effect of different  $\text{N}_2/\text{CO}_2/\text{H}_2\text{O}$  doping ratio in  $\text{CH}_4/\text{air}$  laminar combustion flame. Based on the experimental results, the dependence of the LBV of methane on the equivalence ratio

was also emphasized by Ren et al. [33–35]. Zahedi et al. [36] analyzed the effects of  $N_2$ ,  $CO_2$  and  $H_2$  on LBV and NO formation of  $CH_4$  premixed flames by HFM and numerical simulation. Xiang et al. [37] performed a numerical analysis on the effect of  $CO_2$  on intermediate important free radicals in methane laminar premixed flames. Bougrine et al. [38] used an detailed chemical reaction mechanism to predict the  $(CH_4+H_2)/air$  laminar combustion characteristics under high temperature and pressure condition. The numerical results showed that H plays an indispensable role in leading the main chemical reaction, what's more, adding hydrogen can promote the formation of the important intermediate radical H. Lafay et al. [39] carried out an experimental and numerical investigation on the laminar flame thickness of methane-air mixture with adding hydrogen. It was concluded that the thickness of the laminar flame is reduced by hydrogen addition. Li et al. [40] numerically studied the reaction kinetic mechanism and thermodynamic characteristics of laminar premixed flames of hydrogen-doped methane mixtures. The results reported that hydrogen addition promotes the heat release in the early stage of methane laminar flames and the reaction that hydrogen has the greatest impact on  $OH + H_2 \rightleftharpoons H + H_2O$ , which is the most important reaction for heat release. Ying and Liu [41] reported the dilution characteristics of the substance  $FH_2$  which has hydrogen thermal and transport characteristics and it isn't involved into the chemical reaction by numerical simulation. The effects of 0–40% hydrogen doping on the specific chemical effects of premixed flame temperature, free radical concentration and NO emission of methane laminar flames were discussed. Li et al. [42] investigated the effects of hydrogen addition on the LBVs of  $CH_4$ ,  $C_2H_6$  and  $C_3H_8$  based on the opposed-flow diffusion flame and numerical simulation. They discussed in detail the influence of adding hydrogen existence on the important reactions of LBVs of three fuels and the changes in the molar concentration of major free radicals. Halter et al. applied the classical shadowing method to study the LBV of methane/air at elevated pressure and hydrogen doping in a spherical flame [43]. The laminar and turbulent premixed flame of methane with hydrogen addition were studied by using SPF and pilot flame at high pressure, respectively [44]. In addition, Halter et al. [45] introduced  $FCO_2$  and compared the effects of  $N_2$  and  $CO_2$  on LBVs of methane and iso-octane. Park et al. [46] used an detailed chemical reaction mechanism to study the methane/air counter-flow diffusion flame diluted by hydrogen and water vapor. It was found that the addition of a small amount of water vapor increased the maximum temperature of the flame, inhibited the formation of H and O free radicals, promoted the rise of OH free radical concentration and depressed the formation of NO. Recently, Amar et al. [47] carried out numerical studies on the counter-flow diffusion flame of BG75 (75% $CH_4$  and 25% $CO_2$ )/ $H_2$  mixture. Han et al. [48] conducted an experimental investigation on the LBVs of  $CH_4$  and  $C_2H_6$  at different temperatures by using HFM. The exponential coefficient correlation of the temperature dependence of LBV was deduced through the analysis of total activation energy. Besides, Liu et al. [49] numerically studied the exergy losses in  $CH_4/H_2$  laminar combustion flame, the results showed that minimum exergy loss occurred at the equivalence ratio of 0.9 for different blends. Zhang et al. [50] studied

the exergy losses in  $H_2$  premixed flames with  $Ar/N_2/CO_2$  as diluents, and numerical simulation results showed the thermal effects of diluents are the primary factor influencing the exergy loss.

Hu et al. [51] explored the effects of initial pressure on methane/air ignition delay and LBV were investigated using constant volume incendiary bombs, USC mech [52] and the Aramco mech [53], and summarized up the relationship between ignition delay time and laminar burning velocity. Cai et al. [54] experimentally and numerically investigated the effects of initial pressure on laminar burning velocity and Markstein lengths by using the spherical flame method and the Aramco mechanism [53]. Apart from that, Chen et al. [55] numerically studied the laminar burning velocity and flame structure of methane/ethylene/air mixtures, the results showed that the addition of ethylene increases the concentration of intermediate important free radicals O, OH, H.

From the above research review, it can be found that there are many studies on pure methane, hydrogen-doped methane and pure ethane, which are the most abundant in natural gas. However, the study of hydrogen doping in ethane combustion is rare, and especially, the effect of  $H_2$  dilution on the physical and chemical characteristics of laminar premixed combustion of methane and ethane is still lacking. This work presents the results of the physical and chemical effects of hydrogen on LBVs, AFTs, NHRRs and elementary reactions responsible for temperature changes of methane and ethane under different equivalence ratios.

## Numerical calculation and mechanism validation

In this article, the effects of different hydrogen doping ratios on the laminar premixed flames of methane and ethane were calculated by using the premixed free-propagating flame model based on Chemkin II [56]/Premix Code [57]. In the calculation process, the mixed gas flow rate is regarded as the eigenvalue of the solution of the premixed free-propagating flame, besides, its initial value is kept at  $0.04 \text{ g}/(\text{cm}^2 \cdot \text{s})$ . The multicomponent transport model is used in all operating conditions, and the Soret effect is taken into account. Using adaptive mesh (50 meshes), the maximum number of meshes is set to 500. Gradient  $GRAD = 0.04$ , curvature  $GURV = 0.04$ . Relative and absolute errors are set at  $10^{-4}$  and  $10^{-9}$  respectively in the iteration process. In order to achieve zero gradients for all variables, the one-dimensional computational domain boundary was set from -0.2 cm to 6 or 10 cm to achieve zero gradients for all variables, so that it can satisfy the requirements of simulation.

The formula for calculating the amount of hydrogen mixing is as follows.

$$D_1 = \frac{V_{\text{dilutents}}}{V_{\text{dilutents}} + V_{\text{fuels}}} \quad (1)$$

Where  $V_{\text{diluent}}$  and  $V_{\text{fuels}}$  are volume fractions of hydrogen and fuel, respectively.  $D_1$  represents the proportion of diluent in the fuel/diluent mixture and is generally used to study the effects of different fuel mixtures [40,47,48]. It can also be used to investigate the influence of impurity gases, such as  $CO_2$  and  $N_2$  in fuels (such as biogas) [31,42,58].

In order to select a precise and reasonable combustion mechanism, based on previous research results and previous work, two widely recognized kinetic mechanisms: GRI-Mech 3.0 [58] (containing 325 elementary oxidation and decomposition reactions and 53 species) and San Diego-Mech [59] of the latest revision (containing 268 elementary reactions and 57 species) that can be applied to oxidation combustion of methane and ethane were selected to analyze the laminar premixed combustion characteristics of the hydrogen addition of methane and ethane.

Moreover, to determine the physical and chemical effects of  $H_2$ , three hypothetical substances,  $FH_2$ ,  $FO_2$  and  $FN_2$ , were added to the GRI 3.0 and San Diego models.  $FO_2$  and  $FN_2$  are defined to eliminate the effects of  $H_2$  on combustion chemical reactions of corresponding oxidant components [41]. Correspondingly, the three hypothetical substances have the same thermodynamic and transport properties of  $H_2$ ,  $O_2$  and  $N_2$  respectively, and they are not involved into any chemical reaction and do not play any role in cracking molecules, but only affect the combustion chemical reaction process through dilution effect, specific heat release and three-body collision, just like inert gases. Therefore, the number of elementary reactions in the two mechanisms cannot increase, nor does it affect the calculation results. The modified models of GRI 3.0 mech and San Diego are defined as GRI 3.0\* and San Diego\*, as shown in Table 1.

To verify the rationality and accuracy of the mechanism selected in this paper, Fig. 1 compares the simulation results of LBVs of methane and ethane at 298 K and 1 atm with other scholars experimental results in relevant literature [3,6,14,15,17,21,25,28,42,44,48,60–72].

From Fig. 1 (a), it can be seen that the LBVs of  $CH_4$  calculated by GRI 3.0\* mechanism agrees well with the experimental values at different equivalence ratios. The results from San Diego\* mechanism prediction agree with the experimental values at lean conditions, but are much smaller than the experimental values at stoichiometric and rich conditions. Fig. 1 (b) shows that the general trend of  $C_2H_6$  results simulated by GRI 3.0\* and San Diego\* mechanism is consistent with the experimental values, but the prediction of San Diego\* mechanism is slightly larger than the experimental values at lean combustion and less than the experimental values at rich condition. Thus, compared with the experimental results, the  $CH_4$  and  $C_2H_6$  laminar premixed flames under the condition of different hydrogen doping ratios should be calculated by GRI 3.0\* mechanism.

## Results and discussion

### LBV and AFT at various initial temperatures and pressures

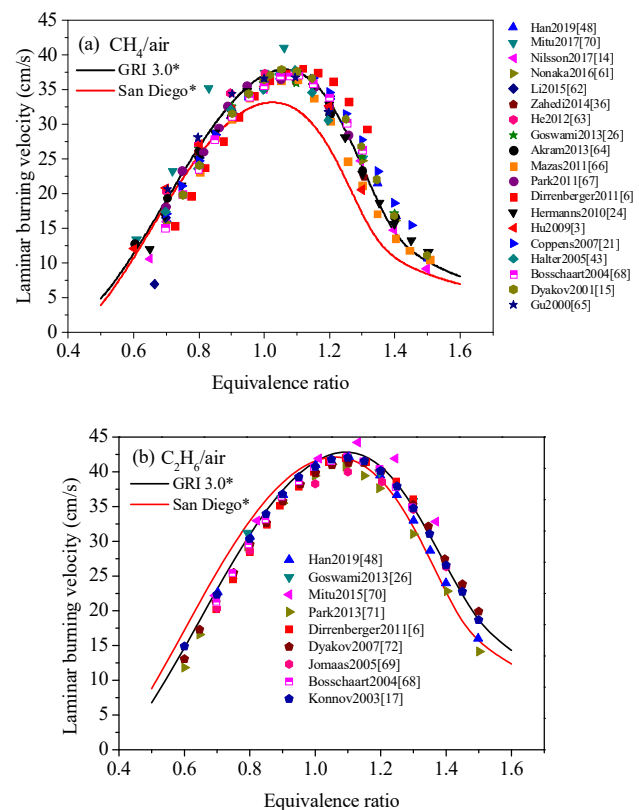
Generally, in industry, before the fuel enters the combustion chamber for combustion, the waste heat generated in the industrial system will be used to preheat the fuel and oxidant in order to save energy and improve the thermal efficiency in fuel combustion. In addition, combustion in internal combustion engine is carried out under high temperature and pressure. Studying laminar premixed combustion of methane and ethane under different initial pressures is helpful to

**Table 1 – Comparison of GRI 3.0 and San Diego mechanism before and after modification.**

Mechanism	Species	Elemental reactions
GRI 3.0	53	325
GRI 3.0*	56	325
San Diego	57	268
San Diego*	60	268

understand the influence of initial parameters on laminar premixed combustion and provide data reference and experimental guidance for combustion in engine cylinder. Fig. 2 gives the LBVs and AFTs of methane and ethane vary with the equivalence ratios at different initial pressures with the initial temperatures 298 K and 473 K, respectively.

The experimental values [26,69] of LBVs of methane and ethane at 298 K, 1, 2 and 5 atm are given in Fig. 2 (a1) and (a2). From Fig. 2 (a1), it is seen that the calculated values of  $CH_4$  at 298 K at different initial pressures agree well with the experimental values measured by HFM [26]. The calculated LBVs of  $C_2H_6$  in Fig. 2 (a2) at room temperature and pressure is in good accordance with the experimental data measured via the counter-flow flame method [71]. When the initial pressure is 2 and 5 atm, the calculated value is slightly overpredicted. Besides, in Fig. 2 (a1) and (a2), it can be found that the LBVs of methane and ethane increase with the increasing of initial temperature, and firstly increase and then decrease with the increase of equivalence ratios. The equivalence ratio of the



**Fig. 1 – Experimental and simulated LBVs at 298 K and 1 atm. (a)  $CH_4$ /air; (b)  $C_2H_6$ /air. (Symbols: experimental data; lines: simulated data).**



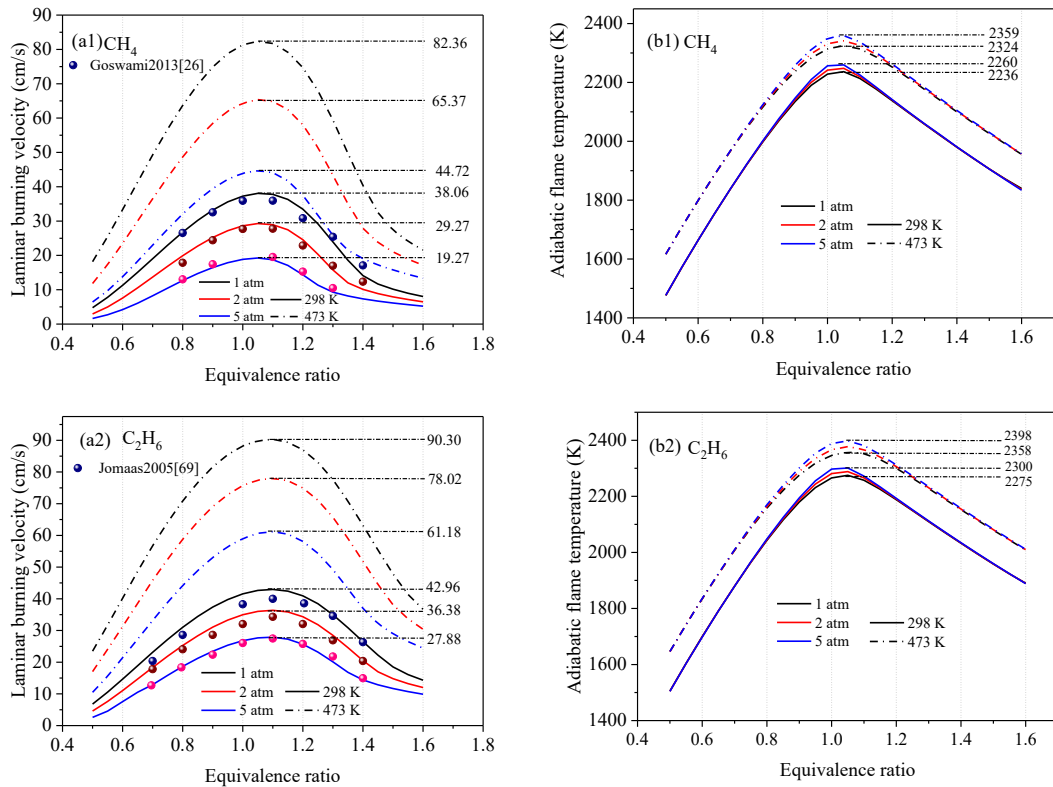


Fig. 2 – Simulated LBVs and AFTs with various initial temperature and pressures.

maximum LBV of CH<sub>4</sub> at different initial temperatures is 1.05, while that of C<sub>2</sub>H<sub>6</sub> is 1.10. Moreover, the LBV of C<sub>2</sub>H<sub>6</sub> is larger than that of CH<sub>4</sub>. With the initial temperature changed from 298 K to 473 K, the LBV of methane and ethane increases by approximately two times.

Fig. 2 (b1) and (b2) show that the AFTs of methane and ethane vary with the equivalence ratio and initial temperature, and the variation trend is consistent with the LBV, but the difference is that the equivalence ratio corresponding to the maximum AFT of two alkanes is 1.05, reflecting the equivalence ratio of the maximum AFT and LBV of C<sub>2</sub>H<sub>6</sub> is different. The AFT of C<sub>2</sub>H<sub>6</sub> is higher than that of CH<sub>4</sub>. When the initial temperature rises from 298 K to 473 K, the AFT of methane and ethane increases by 88 K and 86 K, respectively.

In addition, it can be concluded that from Fig. 2 (a1) and (a2), the LBVs of the two fuels decrease with the increase of pressures at the same temperature. The higher the initial temperature is, the more obvious the effect of pressure on the decrease of LBV is, and the decreasing LBV of CH<sub>4</sub> is the largest when the pressure increases. At the same temperature, the pressure increases from 1 to 5 atm, and the LBV of CH<sub>4</sub> decreases to one-half of the original, while C<sub>2</sub>H<sub>6</sub> decreases to about three-fifths.

It can be concluded from Fig. 2 (b1) and (b2) that the increase of pressure promotes the increasing of AFTs of methane and ethane. For the ranges of equivalence ratios are from 0.8 to 1.2, the change of initial pressure has the significant effect on the AFTs. The higher the initial temperature is, the more obvious the pressure increases the AFT. This is because the increasing of pressure enhances the collision reaction of activating molecules, while the increasing

temperature promotes the cracking of fuel and accelerates the combustion reaction rate, thus increasing the adiabatic flame temperature. It is noteworthy that the change of initial pressure does not affect the corresponding equivalence ratio of maximum LBV and AFT.

#### Effect of hydrogen addition on LBV

##### Comparison on the results of LBV of CH<sub>4</sub> with hydrogen addition

From the first section, we can see that in recent years, domestic and foreign scholars have done a lot of research on CH<sub>4</sub> combustion. Due to the application of natural gas in internal combustion engines, accurate measurement and calculation of LBV of CH<sub>4</sub>-H<sub>2</sub> mixture has become a hot topic in recent years. Fig. 3 is a comparison of the calculated LBV of CH<sub>4</sub> with H<sub>2</sub> addition at room temperature and pressure with the experimental results of Hu et al. (0.1 MPa, 303 K) [3] and Hermanns et al. (1 atm, 298 K) [24]. It can be seen from Fig. 3 that the calculation results of LBVs of CH<sub>4</sub> doped with H<sub>2</sub> are in accord well with those measured by using HFM from Hermanns et al. [24]. Only when the hydrogen ratio is 40%, the calculated value is slightly smaller than that in the laboratory, and overpredicts slightly at rich conditions, but the overall trend is consistent. Due to the inconsistency between the calculation conditions and the results in Hu et al. [3] when measuring SPF with constant volume bomb, the calculated values conforms to the measurements without the hydrogen addition and with hydrogen doping ratio is 20%. When the hydrogen doping ratio is more than 20%, the experimental values are much larger than the calculated values. Compared

with the experimental values of LBVs measured by two methods, it can be further proved that the calculated results in this paper can accurately predict the laminar combustion characteristics of methane and ethane. As shown in Fig. 3, the LBV increases with the increasing of hydrogen content in  $\text{CH}_4/\text{H}_2$ , and the larger the hydrogen doping ratio is, the greater the increase of LBV is. In addition, with the increase of hydrogen doping ratio, the equivalence ratio corresponding to the maximum LBV increases. When the hydrogen doping ratio is less than 20%,  $\Phi = 1.05$ , and when the  $D_1$  is more than 20%,  $\Phi = 1.10$ , which is consistent with the results obtained in Ref. [3]. The influence of hydrogen existence on the LBV of  $\text{CH}_4$  in the rich combustion zone is greater than that in the lean.

The laminar premixed combustion characteristics of fuels are usually affected by mixed combustion of diluents in three ways: (1) the dilution effect due to the decrease in the concentration of the fuel combustion reaction substance with the addition of the diluent; (2) the thermal effect due to the change in the flame temperature; and (3) the chemical effect due to the participation of the diluent in the relevant combustion chemical reaction. In the actual combustion process, these three effects occur simultaneously and are tightly coupled. In this paper, the combined effect of dilution effect and thermal effect on laminar premixed combustion characteristics is defined as “physical effect”. Therefore, the role of the diluent in the combustion chemical reaction is mainly contributed by both physical and chemical effects. The chemical effect of  $\text{H}_2$  on the LBV can be expressed as follows.

$$\Delta S_{L, \text{Chem}} = S_{L, \text{FH}_2} - S_{L, \text{H}_2} \quad (2)$$

Where  $S_{L, \text{FH}_2}$  and  $S_{L, \text{H}_2}$  are the LBV of mixed gas with  $\text{FH}_2$  and  $\text{H}_2$  addition, respectively. The difference  $\Delta S_{L, \text{Chem}}$  between the two represents the effect of the chemical reactivity of  $\text{H}_2$  on the LBV.

The physical effect of  $\text{H}_2$  on LBV can be expressed by:

$$\Delta S_{L, \text{Phys}} = S_{L, 0} - S_{L, \text{FH}_2} \quad (3)$$

Where  $S_{L, 0}$  is the LBV of the mixed gas without  $\text{H}_2$  addition. The difference  $\Delta S_{L, \text{Phys}}$  represents physical effect of  $\text{H}_2$  on the LBV.

If  $\Delta S_{L, \text{Chem}}$  and  $\Delta S_{L, \text{Phys}}$  are positive, the chemical and physical effects of  $\text{H}_2$  decrease the LBV. Conversely, the LBV is increased. The specific effect of methane and ethane blending  $\text{H}_2$  on the LBV is represented by the following formula

$$\Delta S_L = \Delta S_{L, \text{Chem}} \Delta S_{L, \text{Phys}} = \Delta S_{L, 0} - S_{L, \text{H}_2} \quad (4)$$

Where  $\Delta S_L$  indicates the specific effect of blending  $\text{H}_2$  on the LBV of the laminar flames of methane and ethane. If it was positive, hydrogen addition would reduce the LBV, and if it was negative, the LBV would be increased.

Figs. 4 and 5 illustrate the simulation results of LBVs of  $\text{CH}_4$  and  $\text{C}_2\text{H}_6$  with and without  $\text{H}_2$  and  $\text{FH}_2$  addition at 398 K and 1 atm (The calculations are based on this initial temperature and pressure unless otherwise specified) under lean ( $\Phi = 0.8$ ), stoichiometric ( $\Phi = 1.0$ ), rich ( $\Phi = 1.2$ ) combustion conditions.

It can be observed from Fig. 4 (a) that the calculated values of  $\text{CH}_4$  doped with hydrogen agree well with the experimental values [24] with the change of hydrogen doping ratio at  $\Phi = 0.8$ . The LBV of  $\text{CH}_4$  is greatly increased by hydrogen addition, and enhanced by the chemical effect of  $\text{H}_2$ . The LBV

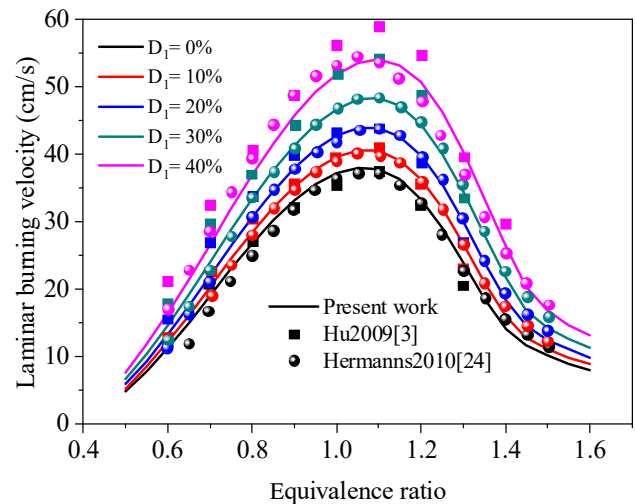


Fig. 3 – Comparison of simulation and experimental results of LBV of  $\text{CH}_4$  with hydrogen addition.

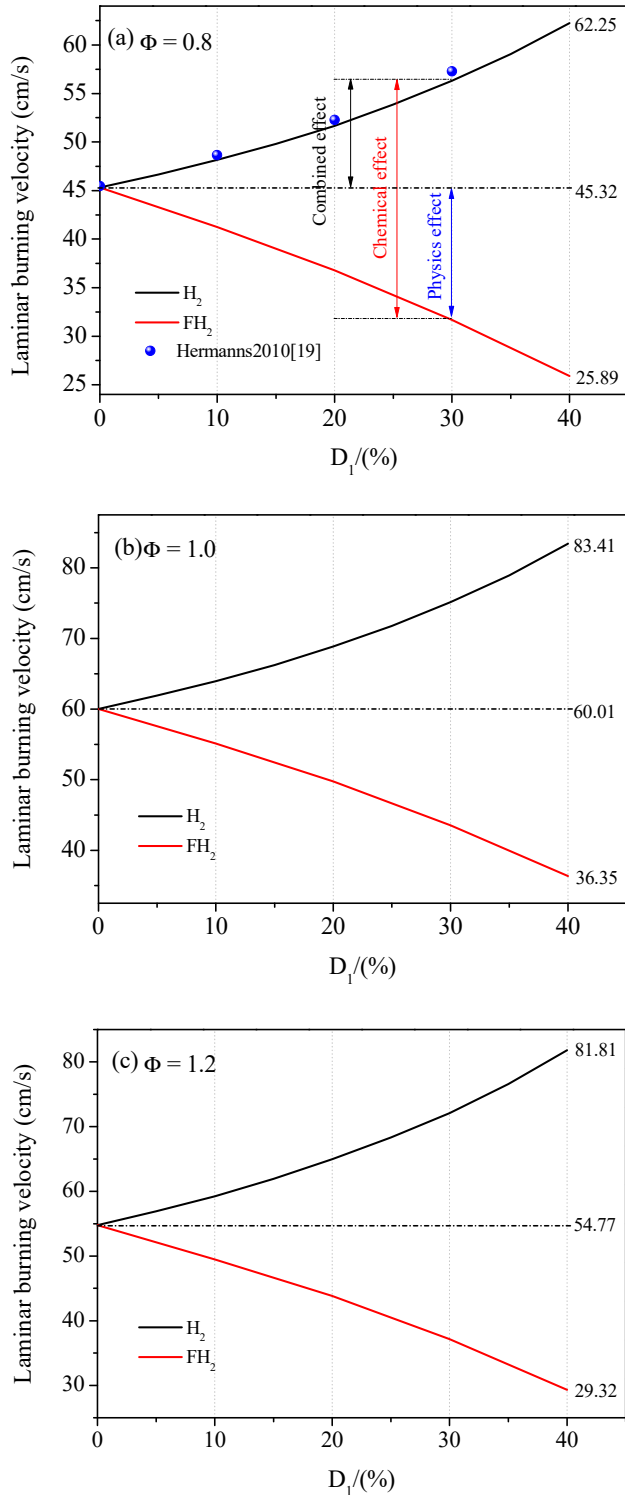
decreases with the physical effect of  $\text{H}_2$ . The chemical effect of  $\text{H}_2$  is twice that of physical effect, so the overall effect of hydrogen doping is to increase the LBV. As shown in Fig. 4 (a)–(c), the chemical effect of  $\text{H}_2$  on LBV increase and the decrease on LBV for  $\text{H}_2$  physical effect are enhanced with the increase of hydrogen doping ratios and equivalence ratios.

From Fig. 5, it is found that the chemical and physical effects of  $\text{H}_2$  addition on the LBV of  $\text{C}_2\text{H}_6$  are consistent with those of  $\text{CH}_4$ . That is to say, the chemical effect of  $\text{H}_2$  promotes the LBV of  $\text{C}_2\text{H}_6$  to increase, while the physical effect reduces the LBV. The effect of  $\text{H}_2$  decreases with the increase of carbon atom number of alkanes [59]. This is mainly due to the high molecular weight of alkanes with more carbon atoms. At the same hydrogen doping ratio, the proportion of  $\text{H}_2$  in the mixture decreases, resulting in the decrease of the combustion chemical dynamic effect. According to literature [3], when the hydrogen doping ratio reaches more than 60%, the main fuel in  $\text{CH}_4\text{--H}_2$  mixture will become  $\text{H}_2$ , meaning that the combustion characteristics of fuel will turn to  $\text{H}_2$ , and the participation of  $\text{CH}_4$  will limit the rapid diffusion of  $\text{H}_2$  combustion.

#### Effect of $\text{H}_2$ and $\text{FH}_2$ on AFT

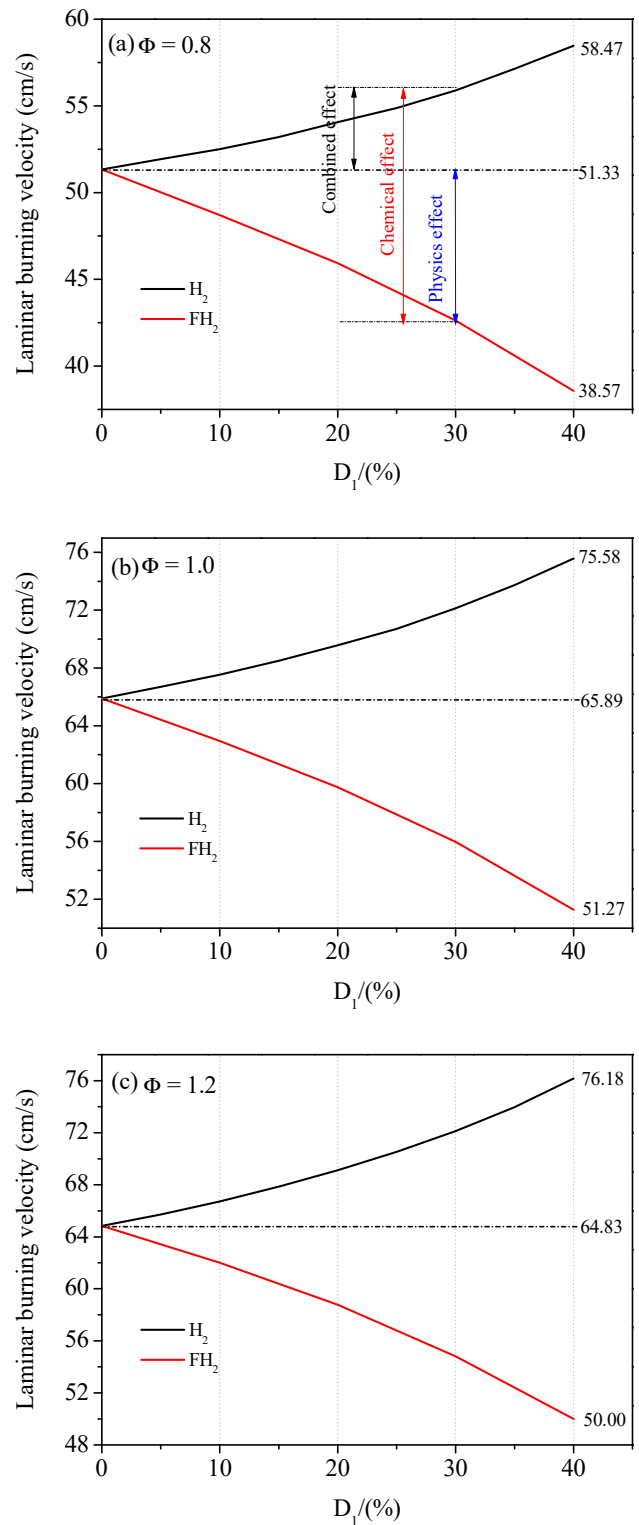
The influence of physical and chemical effects of  $\text{H}_2$  on the AFT and NHRR in the laminar premixed flame of methane and ethane can also be expressed by formulas (2) and (3). It is only necessary to change the laminar combustion parameters in the formulas into corresponding research parameters (such as AFT, NHRR, molar fraction of substance, etc.).

Figs. 6 and 7 show the effects of physical and chemical effects of  $\text{H}_2$  on the AFTs of methane and ethane under lean, stoichiometric and rich conditions. As shown in Figs. 6 (a) and 7 (a), the physical and chemical effects of  $\text{H}_2$  on the AFT are similar to that of LBV. The difference is that the addition of  $\text{H}_2$  has little effect on the rise of AFT, and the physical and chemical effects have little difference. But the combined effect makes the final temperature rise slightly.



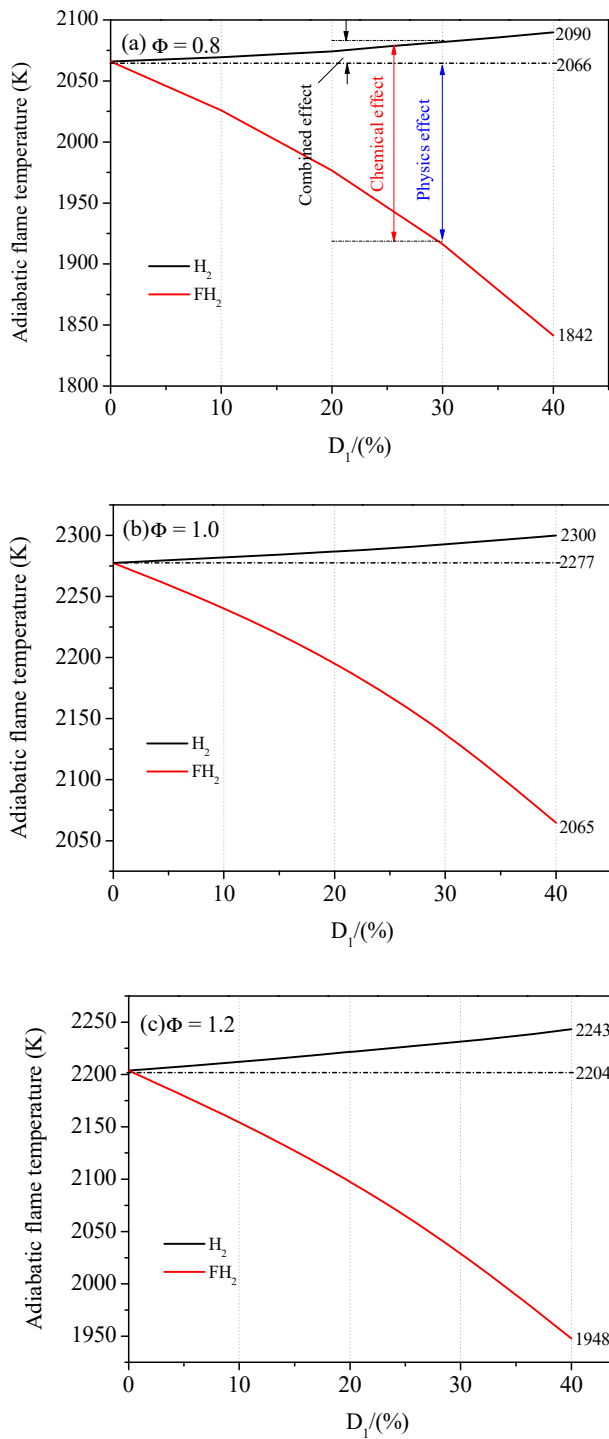
**Fig. 4** – LBVs of CH<sub>4</sub> with H<sub>2</sub> and FH<sub>2</sub> addition at different equivalence ratios.

Compared with Figs. 6 and 7, it is found that the AFT of methane and ethane increases with the increasing of hydrogen doping ratio. Under the same equivalence ratio, the physical and chemical effects of H<sub>2</sub> on the AFT also decrease with the increase of the number of carbon atoms. The chemical effect of H<sub>2</sub> plays a pivotal role in the increase of



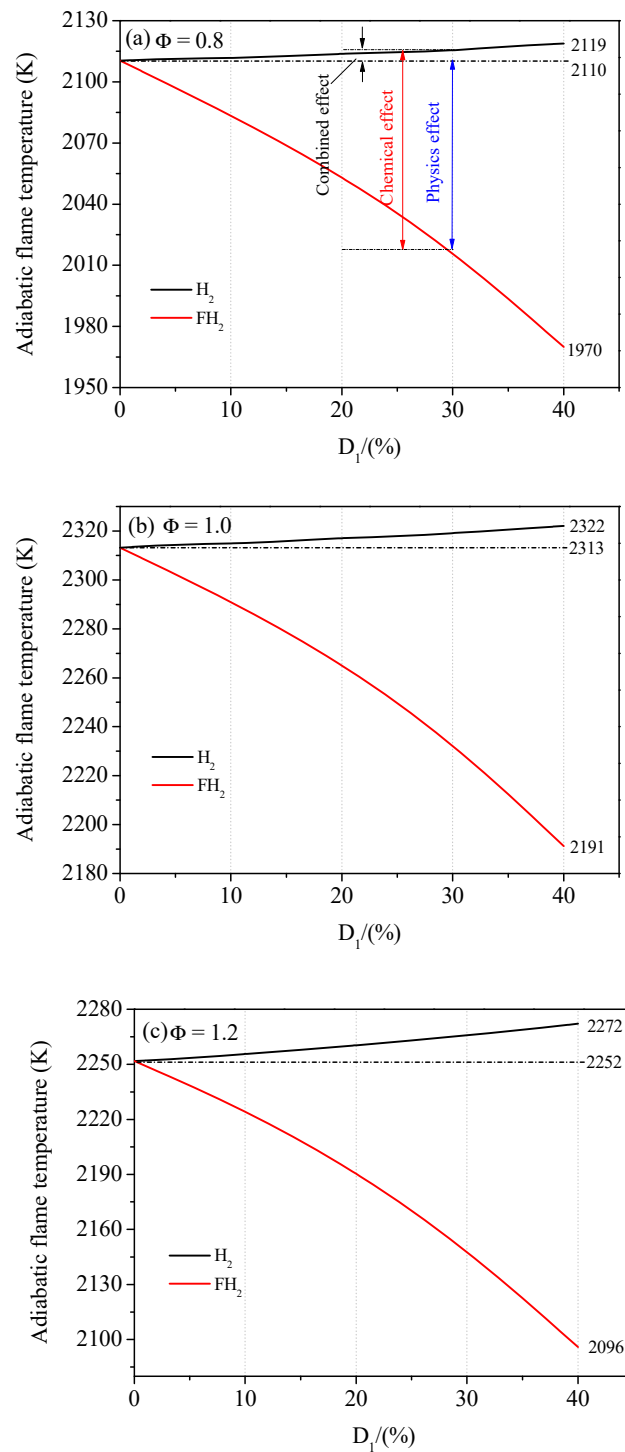
**Fig. 5** – LBVs of C<sub>2</sub>H<sub>6</sub> with H<sub>2</sub> and FH<sub>2</sub> addition at different equivalence ratios.

AFT. The main reason is that H<sub>2</sub> participates in chemical reactions to increase the molar concentration of active free radical pools (O, H, OH, etc.) during combustion process, thus expanding the branched chain reaction in combustion and accelerating the combustion reaction rate [40,58]. In addition,



**Fig. 6** – AFTs of  $\text{CH}_4$  with  $\text{H}_2$  and  $\text{FH}_2$  addition at different equivalence ratios.

for the same fuel, the physical and chemical effects of  $\text{H}_2$  have the greatest impact on LBV and AFT under the rich condition, and the least impact on the stoichiometry. In addition, the addition of  $\text{H}_2$  increased the AFT of  $\text{CH}_4$  most obviously, and the increase of temperature was several times of that of ethane at the same equivalence ratio.



**Fig. 7** – AFTs of  $\text{C}_2\text{H}_6$  with  $\text{H}_2$  and  $\text{FH}_2$  addition at different equivalence ratios.

#### Effect of $\text{H}_2$ and $\text{FH}_2$ on NHRR

As one of the important parameters of laminar combustion characteristic, researching on the heat release rate of fuel has many important implications. For instance, studying the NHRR of fuel has reference value for the later application in



internal combustion engines. The NHRR affects the ignition delay time of the fuel and the design of the internal combustion engine. Besides, the NHRR reflects the amount of energy released by the combustibles in the fire, and the heat release rate of various combustibles is the basis for dividing the fire resistance rating of the building materials, and is an important prerequisite for fire protection design and fire risk assessment. Thus, NHRR comparison has great significance for the future application of fuel. The NHRR reflects the heat generation per unit time in the combustion process, that is, the speed or intensity of chemical reaction in the combustion process. The more intense of the chemical reaction is, the faster the chemical reaction rate is. And the higher the LBV and the AFT are, the higher the NHRR is.

Figs. 8 and 9 show the NHRR of methane and ethane varied with temperature at diverse equivalence ratios and hydrogen doping ratios of 0%, 20% and 40%. It can be found that NHRRs of methane and ethane enhances with the increasing of  $D_1$ . From Figs. 8(a) and 9(a), the flame temperature corresponding to the peak NHRRs decreases with the increase of hydrogen doping ratio when the equivalence ratio is 0.8. That is because with the  $D_1$  increases, the flame combustion reaction begins at a position closer to the nozzle, and the combustion reaction takes place at a lower temperature, indicating that hydrogen doping accelerates the combustion reaction rate. As the hydrogen doping ratio increases, the physical effect of  $H_2$  decreases. Obviously, as the NHRR decreases gradually, the flame temperature corresponding to the peak value decreases gradually. Combined with Effect of  $H_2$  and  $FH_2$  on AFT, the physical effect of  $H_2$  on the temperature drop of AFT is discussed. The physical effect of  $H_2$  inhibits the combustion chemical reaction resulting in the decrease of NHRR. The chemical effect of  $H_2$  accelerates the process of chemical reaction and obviously increases the NHRR of laminar premixed combustion of methane and ethane. At the same equivalence ratio, hydrogen addition has the greatest influence on  $CH_4$ . Moreover, when methane and ethane are mixed with hydrogen, the increase of NHRR is more obvious in the case of rich combustion.

#### Effect of $H_2$ and $FH_2$ on sensitivity analysis

The most forceful and systematic method to quantitatively study the relationship between the model and its parameters is sensitivity analysis. For combustion problems, this method can greatly improve people's insight into the importance of various reaction pathways, so as to achieve the goal of combustion control. In present work, sensitivity analysis was applied to research on the effect of difference hydrogen doping ratio on the temperature of laminar premixed flames of methane and ethane. A more direct understanding of the effects of individual elementary reactions on combustion temperature is conducted. It is of great significance to understand heat release characteristics, to simplify reaction models and to determine control methods. The following formula is used for sensitivity analysis in this paper.

$$c_i(t, l + \Delta l) = c_i(t, l) + \sum_{j=1}^{56} \frac{\partial c_i}{\partial l_j} \Delta l_j + \dots \quad (5)$$

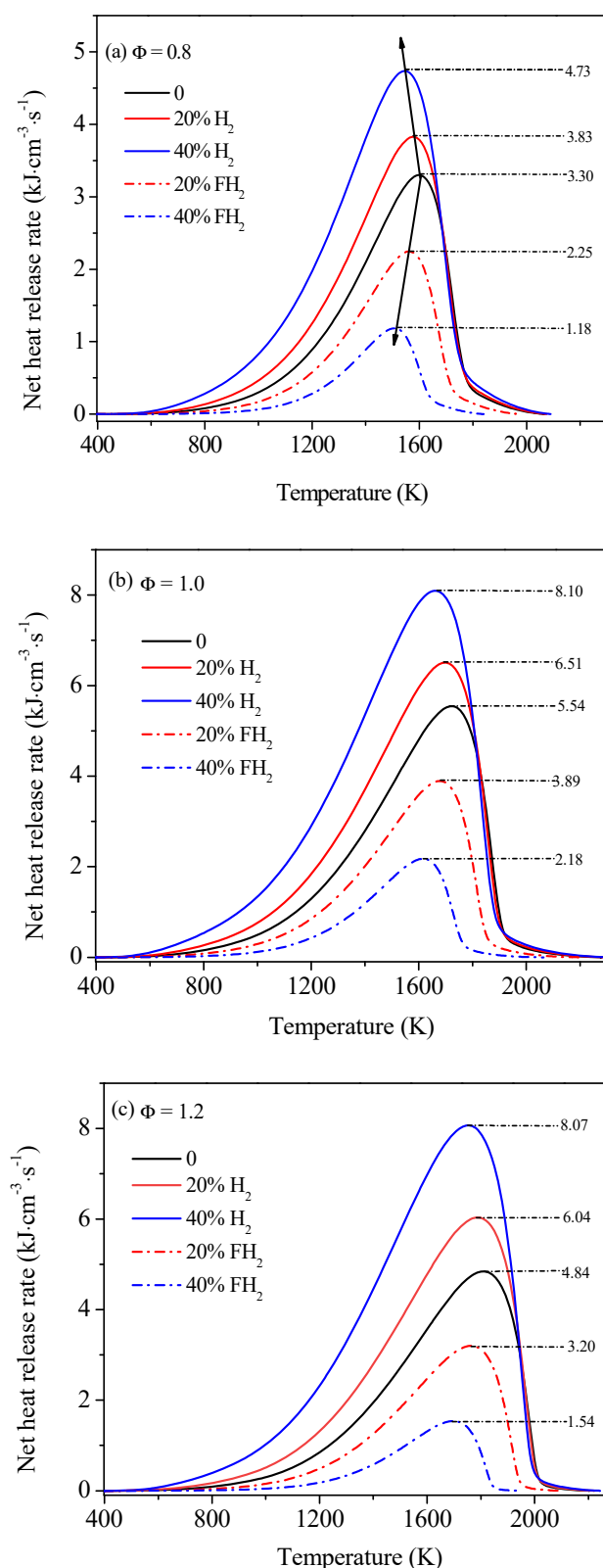


Fig. 8 – NHRRs of  $CH_4$  with  $H_2$  and  $FH_2$  addition at different equivalence ratios.

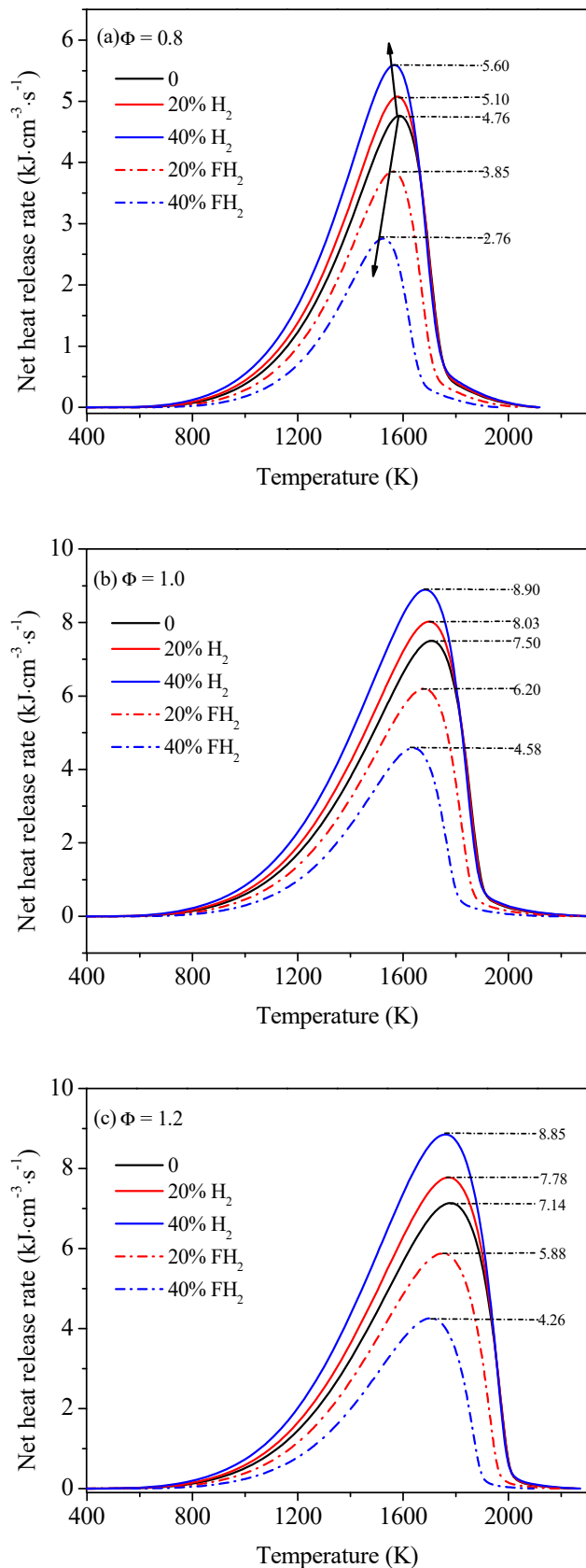


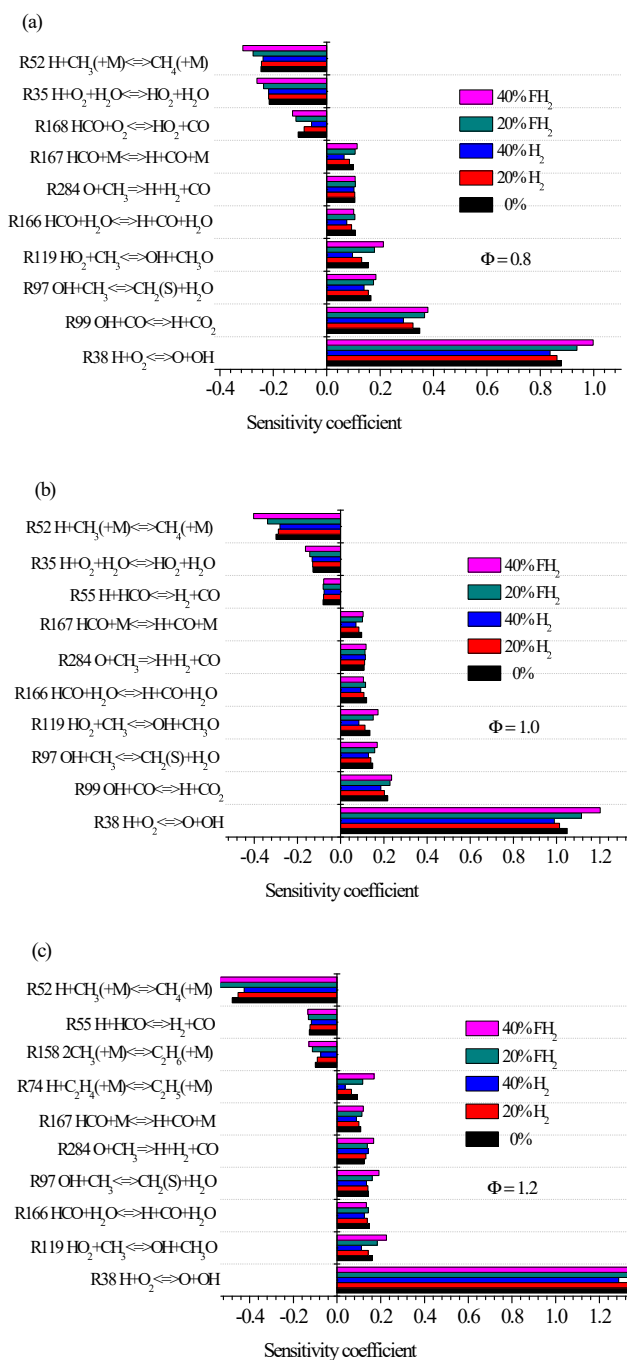
Fig. 9 – NHRRs of  $C_2H_6$  with  $H_2$  and  $FH_2$  addition at different equivalence ratios.

Where  $i$  is the species  $i$  (56 species) and  $c$  is the concentration.  $l$  is the distance from the nozzle,  $\partial c_i / \partial c_j$  is the first-order sensitivity coefficient. So as to study the laminar premixed combustion characteristics of methane and ethane, the first-order sensitivity coefficient of AFT was used to analyze the importance of elementary reactions to laminar premixed flame temperature.

Fig. 10 shows the sensitivity coefficients of  $CH_4$  temperature with  $H_2$  and  $FH_2$  addition at different equivalence ratios. It can be found that in Fig. 10, the most important reaction that promotes the increasing of temperature at different equivalence ratios is  $R38 H + O_2 \rightleftharpoons O + OH$ . It is the most critical elementary reaction in laminar premixed combustion of  $CH_4$  and the initial elementary reaction of branched chain reaction in combustion [39,40,58]. R38 continuously produces active free radicals during the combustion process and promotes the chain reaction, which largely determines the overall combustion reaction rate. With the increasing of  $D_1$ , the dominant effect of R38 on the temperature rise of  $CH_4$  decreases. This is because  $H_2$  participates in combustion chemical reaction and promotes the formation of active free radicals. By comparing with the sensitivity of  $FH_2$  blending, it can be found that  $H_2$  does not participate in chemical reactions, which greatly increases the dependence of temperature rise on R38. The primary reaction that plays a leading role in inhibiting temperature rise is  $R52 H + CH_3(+M) \rightleftharpoons CH_4(+M)$ . The positive direction of R52 is a chain termination reaction, which hinders the development of chain reaction, reducing the combustion reaction rate and inhibiting the temperature rise. With the increasing of hydrogen doping ratio, the effect of R52 on inhibiting temperature rise is weakened, and the dominant effect of  $FH_2$  is increased.

Compared with Fig. 10 (a)–(c), hydrogen addition can increase the inhibition of  $R35 H + O_2 + H_2O \rightleftharpoons HO_2 + H_2O$  on temperature rise at  $\Phi = 1.0$  and enhance the promotion of  $R284 O + CH_3 \rightleftharpoons H + H_2 + CO$  on increasing temperature when the equivalence ratio is 1.2. In other cases, hydrogen doping decreases the sensitivity of important reactions to temperature changes in  $CH_4$  laminar premixed combustion, while  $FH_2$  addition gradually increases the dependence of temperature on the reactions.

The first three elementary reactions which promote and inhibit the rise of  $CH_4$  laminar premixed combustion temperature are different under different equivalence ratios. When the equivalence ratio is 0.8, the first three elementary reactions in the promotion of temperature rise are  $R38 H + O_2 \rightleftharpoons O + OH$ ,  $R99 OH + CO \rightleftharpoons H + CO_2$  and  $R97 OH + CH_3 \rightleftharpoons CH_2(S) + H_2O$ , the first three elementary reactions in inhibition are in turn  $R52 H + CH_3(+M) \rightleftharpoons CH_4(+M)$ ,  $R35 H + O_2 + H_2O \rightleftharpoons HO_2 + H_2O$  and  $R168 HCO + O_2 \rightleftharpoons HO_2 + CO$ . At  $\Phi = 1.0$ , the first three elementary reactions in the promotion effect of temperature rise are the same as those in lean combustion, while one of the elementary reactions for inhibition change from R168 to  $R55 H + HCO \rightleftharpoons H_2 + CO$ . When the equivalence ratio is 1.2, the first three reactions in the promotion for temperature rise are  $R38 H + O_2 \rightleftharpoons O + OH$ ,  $R119 HO_2 + CH_3 \rightleftharpoons OH + CH_3O$  and  $R166 HCO + H_2O \rightleftharpoons H + CO + H_2O$ , while the reactions for the inhibition are R52, R55 and  $R158 2CH_3(+M) \rightleftharpoons C_2H_6(+M)$ . When combustion changes from lean to rich conditions, the content of oxygen decreases



**Fig. 10 – Sensitivity coefficients of  $\text{CH}_4$  temperature with  $\text{H}_2$  and  $\text{FH}_2$  addition at different equivalence ratios.**

relatively, and more  $\text{CH}_3$  and  $\text{H}$  are produced by reaction cracking of  $\text{CH}_4$  and  $\text{H}_2$  in the combustion process, thus reacting with oxygen to produce important intermediate products  $\text{HCO}$  and  $\text{CO}$  in the oxidation combustion reaction of  $\text{CH}_4$ . Therefore, the elementary reactions with different equivalence ratios, which contribute significantly to the laminar premixed combustion temperature of  $\text{CH}_4$ , show the changes in Fig. 10.

When equivalence ratio  $\leq 1$ , with the increase of hydrogen ratio, the chemical effect of hydrogen on promoting effect of R38 and the inhibitory effect on R52 increase. This is because as

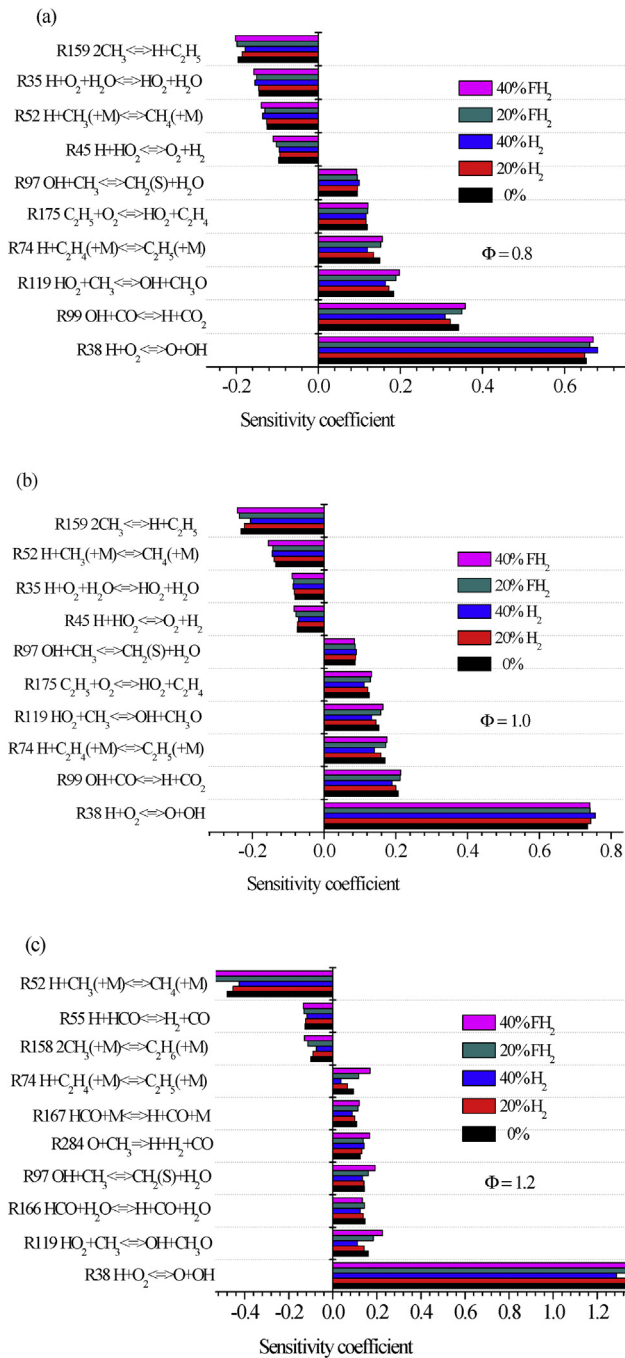
the hydrogen doping ratio increases, the amount of methane decreases, and if hydrogen does not participate in the chemical reaction, methane has sufficient air for the oxidation reaction. The reaction rate of R38 is promoted and the faster decomposition rate of methane produces more  $\text{H}$ , which leads to the positive reaction rate of R52. However, physical effect always promotes the R38 and R52 reaction rate. When equivalence ratio  $> 1$ , chemical and physical effects have little influence on the R38 reaction rate, which means with the increase of hydrogen doping ratio, chemical effect and physical effect have little influence on R38, while chemical effect gradually reduces the influence on R52, while physical effect no longer changes with the hydrogen doping ratio.

Fig. 11 gives the temperature sensitivity coefficients of  $\text{C}_2\text{H}_6$  doped with hydrogen at different equivalence ratios. According to Fig. 11 (a)–(c), the most important reaction that promotes the temperature rise of  $\text{C}_2\text{H}_6$  at different equivalence ratios is  $\text{R38 H} + \text{O}_2 \rightleftharpoons \text{O} + \text{OH}$ , the same as  $\text{CH}_4$ . The difference is that with the increase of  $D_1$ , at  $\Phi = 0.8$ , the effect of R38 on temperature rise first decreases and then increases. Under stoichiometric condition, hydrogen addition increases the promotion of R38, while at  $\Phi = 1.2$ , adding hydrogen decreases the promotion of R38. When the equivalence ratio  $< 1$ , the influence of chemical effect and physical effect on R38 increases with the increase of hydrogen doping ratio. Because the adiabatic flame temperature increases with the increase of hydrogen, which increases the  $\text{H}$  generated by  $\text{H}_2$  and ethane during the oxidation process, leading to the increase of hydrogen to promote the reaction rate of R38. When the equivalence ratio  $\geq 1$ , the chemical effect and the physical effect have little effect on R38 reaction rate. With the increase of hydrogen doping ratio, chemical effects on the inhibition of R52 and R159 reaction rate increase. On the contrary, the promoting effect of physical effect on R159 increases with the increase of hydrogen doping ratio.

In addition, the first three elementary reactions, except R38, promoted the temperature rise of  $\text{C}_2\text{H}_6$  at various equivalence ratios. At  $\Phi = 0.8$ , the order is  $\text{R99 OH} + \text{CO} \rightleftharpoons \text{H} + \text{CO}_2$ ,  $\text{R119 HO}_2 + \text{CH}_3 \rightleftharpoons \text{OH} + \text{CH}_3\text{O}$ . When the equivalence ratio is 1.0, it is  $\text{R99 OH} + \text{CO} \rightleftharpoons \text{H} + \text{CO}_2$ ,  $\text{R74 H} + \text{C}_2\text{H}_4(+\text{M}) \rightleftharpoons \text{C}_2\text{H}_5(+\text{M})$ . At  $\Phi = 1.2$ , it is  $\text{R119 HO}_2 + \text{CH}_3 \rightleftharpoons \text{OH} + \text{CH}_3\text{O}$ ,  $\text{R166 HCO} + \text{H}_2\text{O} \rightleftharpoons \text{H} + \text{CO} + \text{H}_2\text{O}$ .

For the first three important elementary reactions to inhibit the temperature rise of  $\text{C}_2\text{H}_6$ , when the combustion is under lean condition, the reactions are  $\text{R159 } 2\text{CH}_3 \rightleftharpoons \text{H} + \text{C}_2\text{H}_5$ ,  $\text{R35 H} + \text{O}_2 + \text{H}_2\text{O} \rightleftharpoons \text{HO}_2 + \text{H}_2\text{O}$  and  $\text{R52 H} + \text{CH}_3(+\text{M}) \rightleftharpoons \text{CH}_4(+\text{M})$ . At the stoichiometry, they are also R159, R52 and R35, but the sensitivity coefficients changes. At  $\Phi = 1.2$ , the order is  $\text{R52 H} + \text{CH}_3(+\text{M}) \rightleftharpoons \text{CH}_4(+\text{M})$ ,  $\text{R55 H} + \text{HCO} \rightleftharpoons \text{H}_2 + \text{CO}$  and  $\text{R158 } 2\text{CH}_3(+\text{M}) \rightleftharpoons \text{C}_2\text{H}_6(+\text{M})$ . It is noteworthy that R52 suppress temperature rise during rich combustion of  $\text{C}_2\text{H}_6$ . In lean combustion and stoichiometric ratio, R159 produces active  $\text{H}$ , which leads to the increase of  $\text{H}$  concentration in premixed combustion of  $\text{C}_2\text{H}_6$ , thus promoting the overall chemical reaction rate. Maybe this is one of the reasons why the LBV of  $\text{C}_2\text{H}_6$  is faster than methane.

By comparing the blending of  $\text{FH}_2$ , it is seen that the temperature sensitivity of R38 increases when the hydrogen ratio is 40% in lean and stoichiometric conditions, but decreases for



**Fig. 11** – Sensitivity coefficients of  $C_2H_6$  temperature with  $H_2$  and  $FH_2$  addition at different equivalence ratios.

other important elementary reactions. For the same equivalence ratio and hydrogen doping ratio, in addition to R97 in lean and stoichiometric conditions, the addition of  $FH_2$  increases the sensitivity of the elementary reaction that plays a vital role in the temperature change of  $C_2H_6$ .

## Conclusions

Using the premixed free-propagating flame model based on Chemkin II/Premix Code, the influence of  $H_2$  addition

on the combustion characteristics of laminar premixed flame of methane and ethane was systematically studied. Firstly, the effects of different initial temperatures (298–473 K) and pressures (1–5 atm) on LBVs and AFTs of methane and ethane in the equivalence ratio range of 0.5–1.6 were compared and analyzed. Subsequently, the physical and chemical effects of  $H_2$  on LBVs, AFTs, NHRRs and the responsible elementary reactions on temperature rise of methane and ethane laminar premixed flames were discussed under lean ( $\Phi = 0.8$ ), stoichiometric ( $\Phi = 1.0$ ) and rich ( $\Phi = 1.2$ ) conditions at different hydrogen doping ratios (0–40%). The major conclusions are summarized as follows.

- (1) At the same pressure, the LBV and AFT increase with increasing initial temperature. The equivalence ratio of the maximum LBV of  $CH_4$  at different initial temperatures is 1.05, while that of  $C_2H_6$  is 1.10. Different from LBV, the equivalence ratios of maximum AFTs of methane and ethane are 1.05, only the equivalence ratios of maximum AFT and LBV of  $C_2H_6$  are different.
- (2) The LBVs of the two fuels decrease with the increase of pressures at the identical temperature. The higher the initial temperature is, the more obvious the effect of pressure on the decrease of LBV is, and the decreasing LBV of  $CH_4$  is the largest when the pressure increases. At the same temperature, the pressure increases from 1 to 5 atm, and the LBV of  $CH_4$  decreases to 1/2 of the original, while  $C_2H_6$  decreases to about 1/3.
- (3) The effect of hydrogen addition on the LBV of  $CH_4$  in the rich combustion zone is greater than that in the lean. The LBVs of  $CH_4$  and  $C_2H_6$  is greatly increased by hydrogen addition, and enhanced by the chemical effect of  $H_2$ . The LBV decreases with the physical effect of  $H_2$ . The chemical effect of  $H_2$  is twice that of physical effect, so the overall effect of hydrogen doping is to increase the LBV. The effect of  $H_2$  decreases with the increase of carbon atom number of alkanes. The physical and chemical effects of  $H_2$  on the AFT are similar to that of LBV. The difference is that the  $H_2$  addition has slight influence on the changes of AFT.
- (4) The NHRRs of methane and ethane increases with the increasing of hydrogen doping ratio. However, the flame temperature corresponding to the peak of NHRR decreases with the hydrogen doping ratios increase. Compared with  $FH_2$ , the physical effect of  $H_2$  inhibits the combustion chemical reaction, leading to the decrease of NHRR. The chemical effect of  $H_2$  accelerates the process of chemical reaction and obviously improves the NHRR of laminar premixed combustion.
- (5) The two most critical elementary reactions for promoting the temperature rise of methane and ethane are  $H + O_2 \rightleftharpoons OH + O$  and  $CO + OH \rightleftharpoons H + CO_2$ . The important reactions responsible for inhibiting the temperature rise are  $H + CH_3(+M) \rightleftharpoons CH_4(+M)$  and  $H + O_2 + H_2O \rightleftharpoons HO_2 + H_2O$ .



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## REFERENCES

- [1] Demirbas A. Fuel properties of hydrogen, liquefied petroleum gas (LPG), and compressed natural gas (CNG) for transportation. *Energy Sources* 2002;24:601–10.
- [2] Cho H, He B. Spark ignition natural gas engines—a review. *Energy Convers Manag* 2007;48:608–18.
- [3] Hu E, Huang Z, He J, Jin C, Zheng J. Experimental and numerical study on laminar burning characteristics of premixed methane–hydrogen–air flames. *Int J Hydrogen Energy* 2009;34(11):4876–88.
- [4] Wang J, Huang Z, Tang C, Miao H, Wang X. Numerical study of the effect of hydrogen addition on methane–air mixtures combustion. *Int J Hydrogen Energy* 2009;34:1084–96.
- [5] Xu C, Wang H, Zhou K, Li X, Zhou W, Liu W, et al. Laminar burning velocity of premixed ethanol–air mixtures with laser induced spark ignition using constant-volume method. *Energy Fuels* 2019;33:7749–58.
- [6] Dirrenberger P, Le Gall H, Bounaceur R, Herbinet O, Glaude PA, Konnov A, Battin-Leclerc F. Measurements of laminar flame velocity for components of natural gas. *Energy Fuels* 2011;25:3875–84.
- [7] Lamoureux N, Paillard CE. Natural gas ignition delay times behind reflected shock waves: application to modelling and safety. *Shock Waves* 2003;13:57–68.
- [8] Yang W, Liu G, Gong Y, Feng Y. Microbial alteration of natural gas in xinglongtai field of the Bohai Bay basin, China. *Chin. J. Geochem* 2012;31:55–63.
- [9] Chu H, Han W, Cao W, Gu M, Xu G. Effect of methane addition to ethylene on the morphology and size distribution of soot in a laminar co-flow diffusion flame. *Energy* 2019;166:392–400.
- [10] Chu H, Han W, Ren F, Xiang L, Wei Y, Zhang C. Flame synthesis of carbon nanotubes on different substrates in methane diffusion flames. *ES Energy Environ* 2018;2:73–81.
- [11] Farrell JT, Johnston RJ, Androulakis IP. Molecular structure effects on laminar burning velocities at elevated temperature and pressure. *SAE Trans* 2004;1404–25.
- [12] Lowry W, de Vries J, Krejci M, Petersen E, Serinyel Z, Metcalfe W, Curran H, Bourque G. Laminar flame speed measurements and modeling of pure alkanes and alkane blends at elevated pressures. *J Eng Gas Turbines Power* 2011;133(9):091501.
- [13] Olsson JO, Andersson LL. Sensitivity analysis based on an efficient brute-force method, applied to an experimental CH<sub>4</sub>/O<sub>2</sub> premixed laminar flame. *Combust Flame* 1987;67:99–109.
- [14] Nilsson EJK, van Sprang A, Larfeldt J, Konnov AA. The comparative and combined effects of hydrogen addition on the laminar burning velocities of methane and its blends with ethane and propane. *Fuel* 2017;189:369–76.
- [15] Dyakov IV, Konnov AA, Ruyck JD, Bosschaert KJ, Brock EC, De Goey LP. Measurement of adiabatic burning velocity in methane–oxygen–nitrogen mixtures. *Combust Sci Technol* 2001;172:81–96.
- [16] Konnov AA, Dyakov IV, De Ruyck J. Measurement of adiabatic burning velocity and sampling in methane–oxygen–carbon dioxide mixtures. *Arch Combust* 2002;22:13–24.
- [17] Konnov AA, Dyakov IV, De Ruyck J. Measurement of adiabatic burning velocity in ethane–oxygen–nitrogen and in ethane–oxygen–argon mixtures. *Exp Therm Fluid Sci* 2003;27:379–84.
- [18] Konnov AA, Dyakov IV. Measurement of propagation speeds in adiabatic cellular premixed flames of CH<sub>4</sub>+O<sub>2</sub>+CO<sub>2</sub>. *Exp Therm Fluid Sci* 2005;29:901–7.
- [19] Konnov AA, Dyakov IV. Measurement of propagation speeds in adiabatic flat and cellular premixed flames of C<sub>2</sub>H<sub>6</sub>+ O<sub>2</sub>+ CO<sub>2</sub>. *Combust Flame* 2004;136:371–6.
- [20] Konnov AA, Dyakov IV. Experimental study of adiabatic cellular premixed flames of methane (ethane, propane)+ oxygen+ carbon dioxide mixtures. *Combust Sci Technol* 2007;179:747–65.
- [21] Coppens FHV, De Ruyck J, Konnov AA. Effects of hydrogen enrichment on adiabatic burning velocity and NO formation in methane+air flames. *Exp Therm Fluid Sci* 2007;31:437–44.
- [22] Konnov AA, Riemeijer R, De Goey LPH. Adiabatic laminar burning velocities of CH<sub>4</sub>+H<sub>2</sub>+air flames at low pressures. *Fuel* 2010;89:1392–6.
- [23] Konnov AA. The effect of temperature on the adiabatic laminar burning velocities of CH<sub>4</sub>–air and H<sub>2</sub>–air flames. *Fuel* 2010;89:2211–6.
- [24] Hermanns RT, Konnov AA, Bastiaans RJ, De Goey LP, Lucka K, Köhne H. Effects of temperature and composition on the laminar burning velocity of CH<sub>4</sub>+H<sub>2</sub>+O<sub>2</sub>+N<sub>2</sub> flames. *Fuel* 2010;89:114–21.
- [25] Coppens FHV, De Ruyck J, Konnov AA. The effects of composition on burning velocity and nitric oxide formation in laminar premixed flames of CH<sub>4</sub>+H<sub>2</sub>+O<sub>2</sub>+N<sub>2</sub>. *Combust Flame* 2007;149:409–17.
- [26] Goswami M, Derks SC, Coumans K, Slikker WJ, de Andrade Oliveira MH, Bastiaans RJ, Luijten CC, de Goey LP, Konnov AA. The effect of elevated pressures on the laminar burning velocity of methane+ air mixtures. *Combust Flame* 2013;160:1627–35.
- [27] Goswami M, Bastiaans RJM, De Goey LPH, Konnov AA. Experimental and modelling study of the effect of elevated pressure on ethane and propane flames. *Fuel* 2016;166:410–8.
- [28] Hu E, Huang Z, He J, Miao H. Experimental and numerical study on lean premixed methane–hydrogen–air flames at elevated pressures and temperatures. *Int J Hydrogen Energy* 2009;34:6951–60.
- [29] Hu E, Huang Z, He J, Jin C, Zheng J. Experimental and numerical study on laminar burning characteristics of premixed methane–hydrogen–air flames. *Int J Hydrogen Energy* 2009;34:4876–88.
- [30] Wang J, Hu E, Huang Z, Ma Z, Tian Z, Wang J, Li Y. An experimental study of premixed laminar methane/oxygen/argon flames doped with hydrogen at low pressure with synchrotron photoionization. *Chin Sci Bull* 2008;53:1262–9.
- [31] Sun ZY. Laminar explosion properties of syngas. *Combust Sci Technol* 2018;1–16.
- [32] Sun ZY. Experimental studies on the explosion indices in turbulent stoichiometric H<sub>2</sub>/CH<sub>4</sub>/air mixtures. *Int J Hydrogen Energy* 2019;44:469–76.
- [33] Ren F, Chu H, Xiang L, Han W, Gu M. Effect of hydrogen addition on the laminar premixed combustion characteristics the main components of natural gas. *J Energy Inst* 2019;92:1178–90.
- [34] Ren F, Xiang L, Chu H, Ya Y, Han W, Nie X. Numerical investigation on the effect of CO<sub>2</sub> and steam for the H<sub>2</sub> intermediate formation and NO<sub>x</sub> emission in laminar



- premixed methane/air flames. *Int J Hydrogen Energy* 2019. <https://doi.org/10.1016/j.ijhydene.2019.05.096>. online.
- [35] Ren F, Xiang L, Chu H, Jiang H, Ya Y. Modeling study of the impact of blending  $N_2$ ,  $CO_2$ , and  $H_2O$  on characteristics of  $CH_4$  laminar premixed combustion. *Energy Fuels* 2019. <https://doi.org/10.1021/acs.energyfuels.9b02108>. online.
- [36] Zahedi P, Yousefi K. Effects of pressure and carbon dioxide, hydrogen and nitrogen concentration on laminar burning velocities and NO formation of methane-air mixtures. *J Mech Sci Technol* 2014;28:377–86.
- [37] Xiang L, Chu H, Ren F, Gu M. Numerical analysis of the effect of  $CO_2$  on combustion characteristics of laminar premixed methane/air flame. *J Energy Inst* 2019;92:1487–501.
- [38] Bougrine S, Richard S, Nicolle A, Veynante D. Numerical study of laminar flame properties of diluted methane-hydrogen-air flames at high pressure and temperature using detailed chemistry. *Int J Hydrogen Energy* 2011;36:12035–47.
- [39] Lafay Y, Renou B, Cabot G, Boukhalfa M. Experimental and numerical investigation of the effect of  $H_2$  enrichment on laminar methane–air flame thickness. *Combust Flame* 2008;115:540–61.
- [40] Li Q, Hu G, Liao S, Cheng Q, Zhang C, Yuan C. Kinetic effects of hydrogen addition on the thermal characteristics of methane–air premixed flames. *Energy Fuels* 2014;28:4118–29.
- [41] Ying Y, Liu D. Detailed influences of chemical effects of hydrogen as fuel additive on methane flame. *Int J Hydrogen Energy* 2015;40:3777–88.
- [42] Li Z, Cheng X, Wei W, Qiu L, Wu H. Effects of hydrogen addition on laminar flame speeds of methane, ethane and propane: experimental and numerical analysis. *Int J Hydrogen Energy* 2017;42(38):24055–66.
- [43] Halter F, Chauveau C, Djebaili-Chaumeix N, Gökalp I. Characterization of the effects of pressure and hydrogen concentration on laminar burning velocities of methane–hydrogen–air mixtures. *Proc Combust Inst* 2005;30:201–8.
- [44] Halter F, Chauveau C, Gökalp I. Characterization of the effects of hydrogen addition in premixed methane/air flames. *Int J Hydrogen Energy* 2007;32:2585–92.
- [45] Halter F, Foucher F, Landry L, Mounaïm-Rousselle C. Effect of dilution by nitrogen and/or carbon dioxide on methane and iso-octane air flames. *Combust Sci Technol* 2009;181:813–27.
- [46] Park J, Keel SI, Yun JH. Addition effects of  $H_2$  and  $H_2O$  on flame structure and pollutant emissions in methane–air diffusion flame. *Energy Fuels* 2007;21:3216–24.
- [47] Amar H, Abdelbaki M, Fouzi T, Zeroual A. Effect of the addition of  $H_2$  and  $H_2O$  on the polluting species in a counter-flow diffusion flame of biogas in flameless regime. *Int J Hydrogen Energy* 2018;43:3475–81.
- [48] Han X, Wang Z, Wang S, Whiddon R, He Y, Lv Y, Konnov AA. Parametrization of the temperature dependence of laminar burning velocity for methane and ethane flames. *Fuel* 2019;239:1028–37.
- [49] Liu Y, Zhang J, Ju D, Huang Z, Han D. Analysis of exergy losses in laminar premixed flames of methane/hydrogen blends. *Int J Hydrogen Energy* 2019;44:24043–53.
- [50] Zhang J, Han D, Huang Z. Second-law thermodynamic analysis for premixed hydrogen flames with diluents of argon/nitrogen/carbon dioxide. *Int J Hydrogen Energy* 2019;44:5020–9.
- [51] Hu E, Li X, Meng X, Chen Y, Cheng Y, Xie Y, Huang Z. Laminar flame speeds and ignition delay times of methane–air mixtures at elevated temperatures and pressures. *Fuel* 2015;158:1–10.
- [52] Wang H, You X, Joshi AV, Davis SG, Laskin A, Egolfopoulos F, Law CK, Version II UM. High-temperature combustion reaction model of  $H_2/CO/C_1-C_4$  compounds. 2007. [http://ignis.usc.edu/USC\\_Mech\\_II.htm](http://ignis.usc.edu/USC_Mech_II.htm).
- [53] Metcalfe WK, Burke SM, Ahmed SS, Curran HJ. A hierarchical and comparative kinetic modeling study of  $C_1-C_2$  hydrocarbon and oxygenated fuels. *Int J Chem Kinet* 2013;45:638–75.
- [54] Cai X, Wang J, Zhang W, Xie Y, Zhang M, Huang Z. Effects of oxygen enrichment on laminar burning velocities and Markstein lengths of  $CH_4/O_2/N_2$  flames at elevated pressures. *Fuel* 2016;184:466–73.
- [55] Chen S, Jiang Y, Qiu R, An J. Numerical study on laminar burning velocity and flame stability of premixed methane/ethylene/air flames. *Chin J Chem Eng* 2012;20:914–22.
- [56] Kee RJ, Rupley FM, Miller JA. Sandia national laboratories report SAND89-8009B. 1993.
- [57] Kee RJ, Grcar JF, Smooke M, Miller J, Meeks E. Sandia national laboratories report, SAND85-8240. 1985.
- [58] Frenklach M, Bowman CT, Smith GP, Gardiner WC. World wide web location. 1999. <http://www.me.berkeley.edu/gri-mech> >, Version 3.0.
- [59] Chemical-kinetic mechanisms for combustion applications", san Diego mechanism web page, mechanical and aerospace engineering (combustion research). University of California at San Diego, <http://combustion.ucsd.edu>.
- [60] Mitu M, Giurcan V, Razus D, Oancea D. Inert gas influence on the laminar burning velocity of methane-air mixtures. *J Hazard Mater* 2017;321:440–8.
- [61] Nonaka HOB, Pereira FM. Experimental and numerical study of  $CO_2$  content effects on the laminar burning velocity of biogas. *Fuel* 2016;182:382–90.
- [62] Li G, Liang J, Zhang Z, Tian L, Cai Y, Tian L. Experimental investigation on laminar burning velocities and Markstein lengths of premixed methane–n–heptane–air mixtures. *Energy Fuels* 2015;29:4549–56.
- [63] He Y, Wang Z, Yang L, Whiddon R, Li Z, Zhou J, Cen K. Investigation of laminar flame speeds of typical syngas using laser based Bunsen method and kinetic simulation. *Fuel* 2012;95:206–13.
- [64] Akram M, Saxena P, Kumar S. Laminar Burning velocity of methane–air mixtures at elevated temperatures. *Energy Fuels* 2013;27:3460–6.
- [65] Gu XJ, Haq MZ, Lawes M, Woolley R. Laminar burning velocity and Markstein lengths of methane–air mixtures. *Combust Flame* 2000;121:41–58.
- [66] Mazas AN, Fiorina B, Lacoste DA, Schuller T. Effects of water vapor addition on the laminar burning velocity of oxygen-enriched methane flames. *Combust Flame* 2011;158:2428–40.
- [67] Park O, Veloo PS, Liu N, Egolfopoulos FN. Combustion characteristics of alternative gaseous fuels. *Proc Combust Inst* 2011;33:887–94.
- [68] Bosschaart KJ, De Goeij LPH. The laminar burning velocity of flames propagating in mixtures of hydrocarbons and air measured with the heat flux method. *Combust Flame* 2004;136:261–9.
- [69] Jomaas G, Zheng XL, Zhu DL, Law CK. Experimental determination of counterflow ignition temperatures and laminar flame speeds of  $C_2-C_3$  hydrocarbons at atmospheric and elevated pressures. *Proc Combust Inst* 2005;30:193–200.
- [70] Mitu M, Razus D, Giurcan V, Oancea D. Normal burning velocity and propagation speed of ethane–air: pressure and temperature dependence. *Fuel* 2015;147:27–34.
- [71] Park O, Veloo PS, Egolfopoulos FN. Flame studies of  $C_2$  hydrocarbons. *Proc Combust Inst* 2013;34:711–8.
- [72] Dyakov IV, De Ruyck J, Konnov AA. Probe sampling measurements and modeling of nitric oxide formation in ethane + air flames. *Fuel* 2007;86:98–105.